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# The effect of alkaline earth titanates on the rechargeability of manganese dioxide in alkaline electrolyte

M. Kloß, D. Rahner \*, W. Plieth

Dresden University of Technology, Institute of Physical Chemistry and Electrochemistry, 01062 Dresden, Germany

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#### Abstract

Various alkaline earth titanates were tested as the additives for manganese dioxide electrodes in aqueous electrolyte (9 mol/l KOH) at room temperature. The influence of the additives on the discharge capacity of primary cells and especially on cycling behaviour of recha. geable alkaline batteries is discussed. © 1997 Elsevier Science S.A.

Keywords: Alkaline batteries; Manganese dioxide; Alkaline earth titanate

## 1. Introduction

Manganese dioxide is one of the most common cathodic battery materials.  $MnO_2$  is inexpensive, non-toxic and readily available. Starting with the Leclanché cell in 1867 the alkaline Zn/MnO<sub>2</sub> cell is becoming the most used primary battery system. Today,  $\gamma$ -MnO<sub>2</sub> becomes an attractive material for rechargeable cells due to economic and ecological reasons.

The discharge mechanism of  $MnO_2$  in alkaline electrolyte is widely investigated [1–3]. The discharge process occurs in two consecutive discharge steps:

 $MnO_2 + H_2O + e^- \rightarrow MnOOH + OH^-$ (1)

$$MnOOH + H_2O + e^- \rightarrow Mn(OH)_2 + OH^-$$
(2)

The first step, the formation of MnOOH is discussed as a homogeneous solid-phase reaction (Eq. (1)) without changing the basic structure of MnO<sub>2</sub>. During this step, protons arc incorporated into the lattice of MnO<sub>2</sub>. This process is accompanied with reduction of Mn<sup>4+</sup> ions into Mn<sup>3+</sup> ions within the MnO<sub>2</sub> lattice. The corresponding discharge curve follows more or less the Nernst equation and is characterized by a change in the Mn<sup>3+</sup>/Mn<sup>4+</sup> ratio. The discharge reaction is homogeneous and theoretically finished at an oxygen index of x = 1.5 in MnO<sub>4</sub>. In addition to this homogeneous reaction the mechanism for the second discharge step is discussed (Eq. (2)). Parts of the initial solid-phase MnOOH are converted via the liquid phase (formation of  $[Mn(OH)_4]_-^-$  complex ions) into the new solid-phase Mn(OH)<sub>2</sub>. The electrochemical process, therefore, consists mostly of the reduction of  $[Mn(OH)_4]^$ to  $[Mn(OH)_4]^2^-$  on carbon particles of the conductive additive [1]. This deep-discharge limits strongly the rechargeability of MnO<sub>2</sub>.

For ecological and economic reasons it is desirable to create the alkaline manganese cell as a renewable (rechargeable) system [4,5]. The  $MnO_2$  electrode itself will then encounter a lot of elementary problems with respect to sufficient discharge/charge cycleability.

When discharging of MnO<sub>2</sub> continuously beyond the MnOOH level (second discharge step, Eq. (2)), an irreversible phase transition was observed, and the manganese dioxide lost its fully rechargeability. Bode et al. [6] found, that  $\gamma$ -MnO<sub>2</sub> was reduced in a homogeneous phase to MnO<sub>1.6</sub> forming an  $\alpha$ -MnOOH (groutite). This means that the  $\gamma$ -MnO<sub>2</sub> structure remained unchanged. Bell and Huber [7] described a homogeneous phase reduction to a limit corresponding to MnO<sub>1.7</sub>.

The depth-of-discharge (DOD) of  $MnO_2$  therefore should be limited to about 0.5 protons per manganese, i.e.  $MnO_{1.75}$ . in order to realize  $MnO_2$  with sufficient high cycleability.

In practical, rechargeable  $Zn/MnO_2$  cells it is recommended to limit the discharge of  $MnO_2$  to a cut-off voltage

<sup>\*</sup> Corresponding author. Fax: +49 (351) 463 71 64; Tel.: +49 (351) 463 43 69.

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of  $0.9-1.0 \vee [8]$ . Another way to control the reduction stage is the limitation of the capacity of the Zn electrode [9].

In addition to these technical possibilities one may observe a variety of attempts in obtaining a sufficient reversible  $MnO_2$ by means of physical and chemical modification of the  $MnO_2$ raw material.

Kordesch and Gsellmann [10] described the formation of  $\gamma$ -MnO<sub>2</sub> by means of d.c. electrolysis from acid solutions of divalent manganese(II) ions containing titanyl ions (TiO<sup>2+</sup>). An electrode, made by this modified MnO<sub>2</sub>, was shown to be rechargeable up to 100 cycles with a DOD of 33% compared with the theoretical one-electron capacity. The reference material (International Common Sample (ICS) No.2) provided only 42 discharge/charge cycles. Kordesch emphasized that a simple mixture of MnO<sub>2</sub> powder and titanium dioxide powder has no positive effect on the rechargeability.

Wroblowa and co-workers [11,12] described the 'activation' of the  $MnO_2$  by bismuth and lead ions. ICS materials and sodium birnessite (NaMn<sub>3</sub>O<sub>4</sub>) have been modified by means of extensive mechanical mixing with Bi<sub>2</sub>O<sub>3</sub>, Bi<sub>2</sub>S<sub>3</sub> and PbO, respectively. These doped materials possessed a good cycleability at a reactant utilization within 50–95% of the theoretical two-electron capacity. The practical applicability of these results should be questioned because of the very high excess of the conductive additive.

The influence of bismuth oxide on the electrochemical properties of  $MnO_2$  was also investigated by Axmann and Glemser [13]. They found that the cycleability of the, in general, electrocbomically inactive pyrolusite ( $\beta$ -MnO<sub>2</sub>) could be increased by mechanically grinding with Bi<sub>2</sub>O<sub>3</sub> powder. They also proposed a mechanism for the action of the Bi<sub>2</sub>O<sub>3</sub> suggesting a catalytic action. An alternative explanation of the action of Bi<sub>2</sub>O<sub>3</sub> is given in Ref. [14]. It was shown, independently of the starting modification of MnO<sub>2</sub> that in the presence of Bi<sub>2</sub>O<sub>3</sub> MnO<sub>2</sub> is transformed into a birnessite-like  $\delta$ -MnO<sub>2</sub> with a layered structure and that the Bi<sup>3+</sup> ions are blocking the interconnection points between the layers of MnO<sub>6</sub> octahedrons.

Another way to modify  $MnO_2$  has been reported in Ref. [15]. The described method includes mixing of  $MnO_2$  ( $\gamma$ or  $\beta$ -MnO<sub>2</sub>) with an aqueous solution of electrolytes selected from the group consisting of bismuth, lead and copper compounds. Two other methods of chemical modification have been described in Refs. [14,16]. In one method a layered  $\delta$ -MnO<sub>2</sub> was prepared by the sol-gel process. A second preparation procedure used a freeze-drying step and a low temperature decomposition producing a spinel sturcture. Only doped  $\delta$ -MnO<sub>2</sub> showed improved cycleability supporting the mechanism presented in Ref. [14]. However, the practical use of these layered MnO<sub>2</sub> as the electrode material is questionable due to the low cell voltage.

Taucher et al. [17] improved the cycleability of alkaline  $Zn/MnO_2$  cells by means of addition of a barium compound to the cathode mixture. The additives used are barium oxide, barium hydroxide or barium sulfate. It was found that both

the cell capacity and the cumulative capacity increase when the amount of the additive is about 3% of total mass. The mode of additive action is discussed in this way, that the presence of barium compounds in the close vicinity of the cathode material may reduce the access of zinc ions to the  $MnO_2$ , and therefore, the formation of electrochemically inactive hetaerolite (ZnO · Mn<sub>2</sub>O<sub>3</sub>) is substartially lowered. This influence of barium compounds is also described by Bauer [18].

In the work presented here we investigated the discharge behaviour and the rechargeability of  $MnO_2$  electrodes, which contained a physically modified  $MnO_2$ , in an alkaline electrolyte. The 'doped'  $MnO_2$  was produced by physical mixing of  $MnO_2$  powder and an alkaline earth titanate powder.

### 2. Experimental

A commercial available  $MnO_2$  powder was mixed with an alkaline earth titanate powder (CaTiO<sub>3</sub>, SrTiO<sub>3</sub> or BaTiO<sub>3</sub>). The preparated electrodes were combined with a suitable counter electrode (zinc or cadmium) and subjected to the electrochemical measurements.

Both powders,  $MnO_2$  and titanate, were homogenized in the required ratio using a ball mill during at least 8 h. The received product was a physically modified  $MnO_2$ (PM-MnO<sub>2</sub>).

The used  $MnO_2$ , also used as pure reference material, was electrolytic manganese dioxide EMD-TRF (Mitsui Co., Japan) with a  $\gamma$ -structure. The EMD-TRF exhibits a theoretical capacity of 308 mAh/g regarding the one-electron step. The positive electrodes were manufactured from a mixture of PM-MnO<sub>2</sub> with a conductive additive (Lonza graphite KS 75). A Teflon suspension or Teflon powder was added as a binder. An aqueous solution of potassium hydroxide (9 mol/1) was used as the alkaline electrolyte at room temperature.

The first experiments were carried out in an electrochemical standard cell with a platinum counter electrode and a Hg/HgO/KOH (9 mol/l) reference electrode (RE). The wet mixture of MnO<sub>2</sub>, conductive additive and binder was pasted onto a nickel mesh with 1 cm<sup>2</sup> area.

For another series of experiments we combined the  $MnO_2$  electrode with a commercial available zinc or cadmium counter electrode in a button cell, size 2032, see Fig. 1.

For this purpose the mixture of the positive electrode consisted of 40 mg physically modified  $MnO_2$ , 150 mg Lonza graphite KS 75 and 10 mg Teflon powder. This mixture was ground in a mortar and pressed between two nickel meshes into a pellet with a pressure of 30 kN/cm<sup>2</sup>. The obtained electrode pellets were 16 mm in diameter and 1.2 mm in height. The zinc electrode consisted of a porous mercury-free material with a theoretical capacity of 58 mAh/cm<sup>2</sup>. The cadmium electrode (15 mm in diameter) used was 10 times



Fig. 1. Scheme of the button cell.

oversized with a theoretical capacity of 130 mAh at an exploitation of 50%.

We used a separator layer system of polypropylene fleece FS 2123W1 (Freudenberg, Germany), polyvinyl chloride distance holder and microporous polypropylene membrane Celgard 2500 (Hoechst, Germany).

The electrochemical measurements were carried out by means of an EG&G Princeton Applied Research (PAR) 273A potentiostat/galvanostat controlled by PAR M270 electrochemistry software. A special electronic equipment of MACK Elektronik, Germany, was used for galvanostatic cycleability tests.

## 3. Results and discussion

The first measurements were performed in electrochemical standard cells using a high excess of alkaline electrolyte.

Fi. 2 shows the cyclic voltammograms of pasted electrodes with unmodified and BaTiO<sub>3</sub>-modified MnO<sub>2</sub> in the first cycle. The reduction of the  $\gamma$ -MnO<sub>2</sub> progresses in two steps, indicated by two cathodic peaks. Up to a potential of -0.375 V versus RE the reduction process can be described by Eq. (1). The proton insertion was found to expand the MnO<sub>2</sub> lattice [19]. In the second cathodic peak (potentials lower than -0.375 V) the reduction of Mn<sup>3+</sup> species occurs according to Eq. (2). In the reverse scan, one observes the anodic step-wise reoxidation of the Mn<sup>2+</sup> and Mn<sup>3+</sup> species. The addition of BaTiO<sub>3</sub> leads to a better utilization of MnO<sub>2</sub>. Considerably higher specific peak current densities are observed in the cathodic as well as in the anodic scan. The BaTiO<sub>3</sub> additive itself shows no own electrochemical activity within the potential range under investigation.

In the electrochemical standard cell, the discharge/charge behaviour was investigated under galvanostatic conditions.

The electrodes were discharged at a specific current density of 30 mA/g  $MnO_2$  and then charged at the same current density up to a cut-off charge potential of 450 mV versus Hg/HgO/KOH (9 mol/1). The DOD was fixed at 150 mAh/ g  $MnO_2$  (this value corresponds to approximately 49% of the theoretical one-electron capacity).

The discharge potentials for the modified and unmodified materials in various cycles are listed in Table 1.

In the case of the BaTiO<sub>3</sub>-modified  $MnO_2$  the discharge end potential of -400 mV versus RE is reached only in the 25th cycle. With the undoped  $MnO_2$  this value is measured already in the 10th cycle. The barium titanate additive improves the cycleability of  $MnO_2$  electrodes, but the number of cycles is stiil very small.

During the investigation of  $MnO_2$  electrodes in model cells various problems arose, therefore not attaining higher cycle numbers. The  $MnO_2$  electrode undergoes a continuously



Fig. 2. Cyclic voltammograms for BaTiO<sub>3</sub>-modified and unmodified MnO<sub>2</sub> electrodes in the first cycle. Mixture ratio:  $95\% \gamma$ -MnO<sub>2</sub> + 5% BaTiO<sub>3</sub>; electrode composition: 20% active material, 75% graphite, and 5% PTFE. Scan rate = 100  $\mu$ V/s.

Table 1 End discharge potentials vs. cycle number for modified and unmodified  $MnO_2$ ; mixture ratio: 95%  $\gamma$ -MnO<sub>2</sub> + 5% BaTiO<sub>3</sub>; electrode composition: 47.5% active material, 47.5% graphite, and 5% PTFE.  $i = 30 \text{ mA/g MnO}_2$ 

Cycle number	BaTiO <sub>3</sub> -modified MnO <sub>2</sub> E vs. RE (mV)	unmodified $MnO_2$ E vs. RE (mV)	
1	- 159	- 203	
5	- 277	-310	
10	-314	- 400	
15	- 339		
25	- 400		

Table 2 Discharge time of various  $Zn/MnO_2$  button cells,  $i = 20 \text{ mA/g } MnO_2$ 

	Discharge time up to a cut-off voltage (h)		
	1.0 V	0.9 V	0.8 V
Reference cell	12.7	13.5	14.8
SrTiO <sub>3</sub> additive	12.8	14.2	17.3
BaTiO <sub>3</sub> additive	12.7	16.6	17.5

expansion and contraction during cycling tests [20]. Therefore, the resistivity between the graphite and  $MnO_2$  particles increases, depending on the contact of the particles in the pellet.

Another serious problem is the high solubility of manganese(III) ions in the strong alkaline electrolyte [21]. In the oversized electrolyte volume the loss of active material is very important and should not neglected. The dissolved  $Mn^{3+}$  species can be reoxidized and precipitated as  $MnO_2$ particles in the electrolyte. Therefore, the content of the active material in the cathodic mass decreases with time.

In order to diminish these undesired processes we studied the behaviour of our modified  $MnO_2$  samples under practical conditions in button cells with zinc or cadmium counter electrodes. Fig. 3 compares the primary discharge behaviour of the modified  $MnO_2$  samples with the unmodfied reference material. The  $Zn/MnO_2$  cells have been discharged with a specific current density of 20 mA/g  $MnO_2$  up to a cell voltage of 0.5 V.

Fig. 3 shows the discharge curves of the  $Zn/MnO_2$  button cells. An addition of alkaline earth titanates to the  $MnO_2$ 

active mass increases the primary discharge capacities of the test cells. The discharge times versus DOD are listed in Table 2.

The results in Table 2 show that the addition of alkaline earth titanates increase the discharge capacity of  $Zn/MnO_2$ primary cells up to 20% (depending on DOD) compared with an unmodified  $MnO_2$  reference cell. These findings are in good agreement with the results of Davis et al. [22].

In order to test the reversibility of the discharge reaction according to Eq. (1) we subjected the button cells to galvanostatic cycling tests.

For the cycling tests the  $MnO_2$  electrode was combined with a cadmium counter electrode. In this way the formation of an electrochemically inactive hetaerolite ( $ZnO \cdot Mn_2O_3$ ) was prevented during the measurements.

Consequently, the influence of the examined additives on the cycleability of the  $MnO_2$  electrode could be tested without this undesired side reaction.

Cd/MnO<sub>2</sub> cells were discharged at a specific current density of 100 mA/g MnO<sub>2</sub>. The discharge capacity was fixed at 154 mAh/g MnO<sub>2</sub>, i.e. 50% of the theoretical one-electron capacity. Charging was carried out with a current density of  $50 \text{ mA/g MnO}_2$  until compensation of the discharge capacity. Fig. 4 shows the end voltages of the charge and discharge



Fig. 3. Constant-current discharge curves of Zn/MnO<sub>2</sub> button cells with modified and unmodified MnO<sub>2</sub>; mixture ratio: 75%  $\gamma$ -MnO<sub>2</sub> + 25% titanate, and i = 20 mA/g MnO<sub>2</sub>.



Fig. 4. End voltages of discharge/charge vs. cycle number for modified and unmodified MnO2 material tested in button cells.

process versus cycle number. The cell containing the unmodified reference material (EMD-TRF) reaches only 36 cycles at a discharge end voltage of 0.1 V. This result is comparable with the experiments of Kordesch et al. [20], who tested various ICS  $MnO_2$  materials with respect to their cycling behaviour.

The cycling characteristics of the modified  $MnO_2$  are better. Cells with the titanate-modified  $MnO_2$  show discharge end voltages higher than 400 mV in the 60th cycle.

In the first charging steps the end voltages of the charging process at the cells with modified  $MnO_2$  are 100 mV lower than the reference cell. In principle the measured charge end voltages are very high. This means that during the charge process side reactions such as oxygen evolution or formation of manganese ions with a valence state higher than four cannot be excluded.

Therefore, we used a modified charging regime with voltage limitation of the charging process to prevent these side reactions. The charging process was divided into a first constant-current step followed by a constant-voltage step (current-voltage charging regime). The complete test regime consisted of:

Discharge  $i = 100 \text{ mA/g MnO}_2$ , DOD: 50% Charge step 1  $i = 50 \text{ mA/g MnO}_2$  up to a cell voltage of 1.4 V Charge step 2 E = 1.4 V (10 h)

The current and cell voltage versus time during a discharging/charging cycle according to this regime is represented schematically in Fig. 5.

The potential limit of 1.4 V versus  $Cd/Cd(OH)_2$  during charging, which was evaluated by cyclic voltammetric experiments, guarantees prevention of side reactions. The results



Fig. 5. Scheme of current and cell voltage vs. time during the cycling regime with voltage limitation.



Fig. 6. Discharge end voltages vs. cycle number for modified and unmodified MnO2. The button cells were recharged by the current-voltage charging regime.

of the constant-current measurements could be reproduced by this current-voltage charging regime. Fig. 6 shows the discharge behaviour of Cd/MnO<sub>2</sub> button cells using titanate modified MnO<sub>2</sub> electrodes in comparison with a reference cell cycled with the described test regime. In all cases, a charging factor of at least 1.0 could be guaranteed. Therefore, a capacity loss due to incomplete recharging can be excluded.

More than 115 cycles with a DOD of 50% (theoretical one-electron capacity) could be attained with the BaTiO<sub>3</sub>-modified MnO<sub>2</sub> before reaching the chosen discharge limit of 0.1 V. The reference cell (unmodified MnO<sub>2</sub>) delivers only 39 cycles under the same conditions. This corresponds to an increase of about 150% in the rechargeability of the MnO<sub>2</sub> electrode compared with the untreated material.

## 4. Conclusions

The addition of alkaline earth titanates causes a better utilization of  $MnO_2$  during the use in primary batteries. In the presence of these additives the discharge/charge cycleability of  $MnO_2$  is clearly improved.

It is still an open question whether the mechanism of these new additives is similar to  $Bi_2O_3$ . The mechanism of the action of the described additives is under investigation.

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